

Amendments to the Claims:

This listing of claims will replace all prior versions, and listings of claims in the application. For the Examiner's convenience, and in view of the proximity to the Amendment submitted on March 21, 2007, the claims below show the amendments made in the Amendment of March 21, 2007 in addition to the amendments made herein.

Listing of Claims:

- 1 1. (Currently Amended) A multi-stage process for the treatment of organic
2 waste comprising:
 - 3 ~~One)~~ **(a)** Drying said waste to reduce ~~the~~ water content to below 15%;
 - 4 ~~Two)~~ **(b)** Subjecting said dried waste to a thermochemical liquefaction
5 process in the presence of a recirculating solvent medium at a temperature of about 275°C to
6 375°C and a pressure of up to 10 atmospheres, thereby obtaining gaseous, liquid and solid
7 products;
 - 8 ~~Three)~~ **(c)** Separating ~~the a~~ formed slurry product from condensable gas,
9 water and other liquid fractions boiling out at up to 250°C;
 - 10 ~~Four)~~ **(d)** Transferring said slurry product obtained from thermal extraction
11 from step c to a pyrolysis apparatus and treating the same at a temperature of about 350°C to
12 500°C to cause additional thermal destruction of unconvertible organic matter of feed material
13 and heavy liquid fractions obtained in step c and their evaporation and removal from pyrolysis
14 apparatus;
 - 15 ~~Five)~~ **(e)** Separating vapor products from condensable oil products;
 - 16 ~~Six)~~ **(f)** Vacuum distillation of oil products from step [~~a~~] **e** for the removal
17 of fractions having a boiling temperature of between 250°C and 350°C; and
 - 18 ~~Seven)~~ **(g)** Recirculating a fraction having a boiling temperature of above
19 300°C as the recirculating solvent medium for step b.

1 2. (Original) A multi-stage process according to claim 1 wherein said
2 recirculating solvent medium is in itself a liquid product with a boiling temperature of above
3 300°C.

1 3. (Original) A multi-stage process according to claim 1 wherein said
2 recirculating solvent medium serves as a hydrogen donor in step b.

1 4. (Original) A multi-stage process according to claim 1 wherein said
2 organic waste, is sewage sludge.

1 5. (Original) A multi-stage process according to claim 1 wherein said waste
2 is dried to reduce the water content to below 12%.

1 6. (Currently Amended) A multi-stage process according to claim 1 wherein
2 the ~~ratio of solvent to sewage sludge feed is~~ solvent and dried waste are present in a ratio of
3 between 0.75:1 and 1.5:1.

1 7. (Currently Amended) A multi-stage process according to claim 1 wherein
2 the ~~ratio of solvent to sewage sludge feed is~~ solvent and dried waste are present in a ratio of
3 about 1:1.

1 8. (Original) A multi-stage process according to claim 1. wherein step d is
2 carried out at a temperature of about 450°C.

1 9. (Currently Amended) A multi-stage process according to claim 1 wherein
2 step [d] g is carried out by recirculating a fraction having a boiling temperature of above 350°C
3 as the recirculating solvent medium for step b.